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stratified because the 20.0 percent criterion for a 3-point test is not met, locate and sample the non-reactive, non-native gas from traverse points for the test in accordance with Sections 11.2 and 11.3 of EPA Method 1 in 40 CFR part 60, Appendix A-1. A minimum of 40 non-reactive gas concentration measurements will be collected at three to five different injected non-reactive gas flow rates for determination of point-of-use abatement device effluent flow. The total volume flow of the point-of-use abatement device exhaust will be calculated consistent with the EPA 430-R-10-003 (incorporated by reference, see § 98.7) Equations 1 through 7.

(3) You must determine the measurement system response time according to paragraphs (c)(3)(i) through (iii) of this appendix.

(i) Before sampling begins, introduce ambient air at the probe upstream of all sample condition components in system calibration mode. Record the time it takes for the measured concentration of a selected compound (for example, carbon dioxide) to reach steady state.

(ii) Introduce nitrogen in the system calibration mode and record the time required for the concentration of the selected compound to reach steady state.

(iii) Observe the time required to achieve 95 percent of a stable response for both nitrogen and ambient air. The longer interval is the measurement system response time.

[78 FR 68234, Nov. 13, 2013]

Subpart J [Reserved]

Subpart K—Ferroalloy Production

§ 98.110 Definition of the source category.

The ferroalloy production source category consists of any facility that uses pyrometallurgical techniques to produce any of the following metals: ferrochromium, ferromanganese, ferromolybdenum, ferronickel, ferrosilicon, ferrotitanium, ferrotungsten, ferrovanadium, silicomanganese, or silicon metal.

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§ 98.111 Reporting threshold.

You must report GHG emissions under this subpart if your facility contains a ferroalloy production process and the facility meets the requirements of either § 98.2(a)(1) or (2).

§ 98.112 GHGs to report.

You must report:

(a) Process CO₂ emissions from each electric arc furnace (EAF) used for the production of any ferroalloy listed in § 98.110, and process CH₄ emissions from each EAF that is used for the production of any ferroalloy listed in Table K-1 to subpart K.

(b) CO₂, CH₄, and N₂O emissions from each stationary combustion unit following the requirements of subpart C of this part. You must report these emissions under subpart C of this part (General Stationary Fuel Combustion Sources).

[74 FR 56374, Oct. 30, 2009, as amended at 75 FR 66461, Oct. 28, 2010]

§ 98.113 Calculating GHG emissions.

You must calculate and report the annual process CO₂ emissions from each EAF not subject to paragraph (c) of this section using the procedures in either paragraph (a) or (b) of this section. For each EAF also subject to annual process CH₄ emissions reporting, you must also calculate and report the annual process CH₄ emissions from the EAF using the procedures in paragraph (d) of this section.

(a) Calculate and report under this subpart the process CO₂ emissions by operating and maintaining CEMS according to the Tier 4 Calculation Methodology in § 98.33(a)(4) and all associated requirements for Tier 4 in subpart C of this part (General Stationary Fuel Combustion Sources).

(b) Calculate and report under this subpart the annual process CO₂ emissions using the procedure in either paragraph (b)(1) or (b)(2) of this section.

(1) Calculate and report under this subpart the annual process CO₂ emissions from EAFs by operating and maintaining a CEMS according to the Tier 4 Calculation Methodology specified in § 98.33(a)(4) and the applicable requirements for Tier 4 in subpart C of

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this part (General Stationary Fuel Combustion Sources).

(2) Calculate and report under this subpart the annual process CO₂ emissions from the EAFs using the carbon mass balance procedure specified in paragraphs (b)(2)(i) and (b)(2)(ii) of this section.

(i) For each EAF, determine the annual mass of carbon in each carbon-containing input and output material for the EAF and estimate annual proc-

ess CO₂ emissions from the EAF using Equation K-1 of this section. Carbon-containing input materials include carbon electrodes and carbonaceous reducing agents. If you document that a specific input or output material contributes less than 1 percent of the total carbon into or out of the process, you do not have to include the material in your calculation using Equation K-1 of this section.

$$\begin{aligned}
 E_{\text{CO}_2} = & \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^i \left(M_{\text{reducing agent}_i} \times C_{\text{reducing agent}_i} \right) \\
 & + \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^m \left(M_{\text{electrode}_m} \times C_{\text{electrode}_m} \right) \\
 & + \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^h \left(M_{\text{ore}_h} \times C_{\text{ore}_h} \right) \\
 & + \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^j \left(M_{\text{flux}_j} \times C_{\text{flux}_j} \right) \\
 & - \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^k \left(M_{\text{product outgoing}_k} \times C_{\text{product outgoing}_k} \right) \\
 & - \frac{44}{12} \times \frac{2000}{2205} \times \sum_1^l \left(M_{\text{non-product outgoing}_l} \times C_{\text{non-product outgoing}_l} \right)
 \end{aligned}
 \tag{Eq. K-1}$$

Where:

E_{CO_2} = Annual process CO₂ emissions from an individual EAF (metric tons).

44/12 = Ratio of molecular weights, CO₂ to carbon.

2000/2205 = Conversion factor to convert tons to metric tons.

$M_{\text{reducing agent}_i}$ = Annual mass of reducing agent i fed, charged, or otherwise introduced into the EAF (tons).

$C_{\text{reducing agent}_i}$ = Carbon content in reducing agent i (percent by weight, expressed as a decimal fraction).

$M_{\text{electrode}_m}$ = Annual mass of carbon electrode m consumed in the EAF (tons).

$C_{\text{electrode}_m}$ = Carbon content of the carbon electrode m (percent by weight, expressed as a decimal fraction).

M_{ore_h} = Annual mass of ore h charged to the EAF (tons).

C_{ore_h} = Carbon content in ore h (percent by weight, expressed as a decimal fraction).

M_{flux_j} = Annual mass of flux material j fed, charged, or otherwise introduced into the EAF to facilitate slag formation (tons).

C_{flux_j} = Carbon content in flux material j (percent by weight, expressed as a decimal fraction).

M_{product_k} = Annual mass of alloy product k tapped from EAF (tons).

C_{product_k} = Carbon content in alloy product k (percent by weight, expressed as a decimal fraction).

$M_{\text{non-product outgoing}_l}$ = Annual mass of non-product outgoing material l removed from EAF (tons).

$C_{\text{non-product outgoing}_l}$ = Carbon content in non-product outgoing material l (percent by weight, expressed as a decimal fraction).

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(ii) Determine the combined annual process CO₂ emissions from the EAFs at your facility using Equation K-2 of this section.

$$\text{CO}_2 = \sum_1^k E_{\text{CO}_2 k} \quad (\text{Eq. K-2})$$

Where:

CO₂ = Annual process CO₂ emissions from EAFs at facility used for the production of any ferroalloy listed in § 98.110 (metric tons).

E_{CO₂k} = Annual process CO₂ emissions calculated from EAF *k* calculated using Equation K-1 of this section (metric tons).

k = Total number of EAFs at facility used for the production of any ferroalloy listed in § 98.110.

(c) If GHG emissions from an EAF are vented through the same stack as any combustion unit or process equipment that reports CO₂ emissions using

a CEMS that complies with the Tier 4 Calculation Methodology in subpart C of this part (General Stationary Fuel Combustion Sources), then the calculation methodology in paragraph (b) of this section shall not be used to calculate process emissions. The owner or operator shall report under this subpart the combined stack emissions according to the Tier 4 Calculation Methodology in § 98.33(a)(4) and all associated requirements for Tier 4 in subpart C of this part.

(d) For the EAFs at your facility used for the production of any ferroalloy listed in Table K-1 of this subpart, you must calculate and report the annual CH₄ emissions using the procedure specified in paragraphs (d)(1) and (2) of this section.

(1) For each EAF, determine the annual CH₄ emissions using Equation K-3 of this section.

$$E_{\text{CH}_4} = \sum_1^j (M_{\text{product } i} \times \frac{2}{2205} \times EF_{\text{product } i}) \quad (\text{Eq. K-3})$$

Where:

E_{CH₄} = Annual process CH₄ emissions from an individual EAF (metric tons).

M_{product_i} = Annual mass of alloy product *i* produced in the EAF (tons).

2/2205 = Conversion factor to convert kg CH₄/ton of product to metric tons CH₄.

EF_{product_i} = CH₄ emission factor for alloy product *i* from Table K-1 in this subpart (kg of CH₄ emissions per metric ton of alloy product *i*).

(2) Determine the combined process CH₄ emissions from the EAFs at your facility using Equation K-4 of this section:

$$\text{CH}_4 = \sum_1^j E_{\text{CH}_4 j} \quad (\text{Eq. K-4})$$

Where:

CH₄ = Annual process CH₄ emissions from EAFs at facility used for the production of ferroalloys listed in Table K-1 of this subpart (metric tons).

E_{CH₄j} = Annual process CH₄ emissions from EAF *j* calculated using Equation K-3 of this section (metric tons).

j = Total number of EAFs at facility used for the production of ferroalloys listed in Table K-1 of this subpart.

[74 FR 56374, Oct. 30, 2009, as amended at 75 FR 66461, Oct. 28, 2010; 78 FR 71954, Nov. 29, 2013]

§ 98.114 Monitoring and QA/QC requirements.

If you determine annual process CO₂ emissions using the carbon mass balance procedure in § 98.113(b)(2), you must meet the requirements specified in paragraphs (a) and (b) of this section.

(a) Determine the annual mass for each material used for the calculations of annual process CO₂ emissions using Equation K-1 of this subpart by summing the monthly mass for the material determined for each month of the calendar year. The monthly mass may be determined using plant instruments used for accounting purposes, including either direct measurement of the quantity of the material placed in the unit or by calculations using process operating information.